# Runge-Kutta method for flow of dusty fluid along exponentially stretching cylinder

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**Abstract.** The present manuscript focuses on the flow and heat transfer of the dusty fluid along exponentially stretching cylinder. Enormous attempts are made for fluid flow along cylinder but the study of fluid behavior along exponentially stretching cylinder is discussed lately. Using appropriate transformations, the governing partial differential equations are converted to non-dimensional ordinary differential equations. The transformed equations are solved numerically using Shooting technique with Runge-Kutta method. The influence of the physical parameters on the velocity and temperature profiles as well as the skin fraction coefficient and the local Nusselt number are examined in detail. The essential observations are as the fluid velocity decreases but temperature grows with rise in particle interaction parameter, and both the fluid velocity and temperature fall with increase in mass concentration parameter, Reynold number, Particle interaction parameter for temperature and the Prandtl number.

Keywords: dusty fluid; stretching cylinder; exponential stretching; shooting method; numerical solution

### 1. Introduction

Fluid flow behavior along the stretching cylinder in various physical conditions has gained considerable attention over the past few decades. Reasons behind the great interest are its several implementations in many advance industrial techniques such as composite processing, gas cooling systems, processing of plastic foam, polymer technology, watering system channels, cement process industry and many more. Firstly, Wang 1988 studied the fluid behavior along the stretching cylinder. The detailed study of fluid flow along the stretched cylinder for the boundary layer was made (Ishak and Nazar 2009) regarding. Wang (2011) obtained asymptotic solutions for high Reynold number using slip flow condition. Mixed convection condition together with slip flow and obtained numerical solution for the boundary layer problem of Williamson fluid flow over a stretching cylinder

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Copyright © 2020 Techno-Press, Ltd. http://www.techno-press.org/?journal=scs&subpage=8 (Salahuddin *et al.* 2017). The effects of Soret and Dufour for the Casson fluid by considering the heat transfer along stretching cylinder was worked out (Mahdy 2015). The mass and convective heat conditions for Casson fluid flow having nanoparticles along stretching cylinder was presented (Maria *et al.* 2016). A thorough numerical study of sisko fluid flow over stretching cylinder with effects of thermal conductivity and viscous dissipation was done (Malik *et al.* 2016). Al-Maliki et al. (2020) carried out the dynamic analysis of functionally graded (FG) graphenereinforced beams under thermal loading based on finite element approach. The presented formulation is based on a higher order refined beam element accounting for shear deformations. The graphene-reinforced beam is exposed to transverse periodic mechanical loading.

The uniform suction/blowing effects together with transfer of heat outside the permeable stretching cylinder were considered (Ishaq *et al.* 2008). Under convective boundary conditions, electrically conducting sisko fluid along the stretching cylinder in axial direction was probed (Khan and Malik 2015). They found the considerable boost in the flow parameters for shear thinning than thickening. The notable point about all the above mentioned studies is

that the considered fluid is "Pure". Practically it is almost impossible to have such fluid which is free from any kind of impurity. Every naturally occurring fluid contains dust particles. Many engineering and industrial problems deal with dusty fluid such as powder mechanization and centrifugal technique to the detachment of particles from the fluid. Flow of dusty fluid can be viewed in many natural phenomena e.g., flow of mud in rivers, blood flow and atmospheric flow during haze. Initiative study of motion of dust particles in laminar flow has been carried out (Saffman, 1962). An analysis for viscous, incompressible steady flow of dusty fluid flowing between two co-axial rotating cylinders under pressure gradient effect was carried out (Girishwar 1970). Akgoz and Civalek (2011) investigated geometrically the nonlinear free vibration analysis of thin laminated plates resting on non-linear elastic foundations. Winkler-Pasternak type foundation model is used. Governing equations of motions are obtained using the von Karman type nonlinear theory. The method of discrete singular convolution is used to obtain the discretised equations of motion of plates. Sharma et al. (2018e) presented the novel higher-order coupled finite-boundary element scheme for the computation of the thermoacoustic responses of the layered panel structure under the harmonic excitation. The thermally pre-stressed vibrating composite panel model is derived mathematically using the higherorder shear deformation mid-plane kinematics. Batou et al. (2019) studied the wave propagations in sigmoid functionally graded (S-FG) plates using new Higher Shear Deformation Theory (HSDT) based on two-dimensional (2D) elasticity theory. The current higher order theory has only four unknowns, which mean that few numbers of unknowns, compared with first shear deformations and others higher shear deformations theories and without needing shear corrector.

Baaskaran et al. (2018) studied the reliable and accurate method of computationally aided design processes of advanced thin walled structures in automotive industries for the efficient usage of smart materials, that possess higher energy absorption in dynamic compression loading. The most versatile components ie, thin walled crash tubes with different geometrical profiles are introduced in view of mitigating the impact of varying cross section in crash behavior and energy absorption characteristics. Sharma et al. (2018c, d) carried out numerically the acoustic radiation responses of doubly curved laminated composite shell panels subjected to harmonic excitation are investigated numerically in the framework of the higherorder shear deformation theory. A general mathematical model for the vibrating curved panel has been developed spherical, and the cylindrical, elliptical and hyperboloid shell panel geometries resting on an infinite rigid baffle are considered for analysis. A numerical scheme for the vibrating plate has been developed in the frame work of the higher-order mid-plane kinematics and the eigen frequencies are obtained by employing suitable finite element steps. Dusty gas flow in a region occupied by boundary layer was examined (Chakrabarti 1974). The coefficient of friction and heat transfer for dusty boundary layer flow with pressure gradient was studied (Agranat

1988). In addition to these studies for flow and transfer of heat for dusty fluid along sheet / surface, many researchers considered dusty fluid flow along cylinder. The viscous, incompressible gas flow having dust particles for an isothermal cylinder was discussed and results from various physical parameters were presented (Rebhi 2010). Chen et al. (2019a, b) carried the energy absorption characteristics of a lattice-web reinforced composite sandwich cylinder (LRCSC) which is composed of glass fiber reinforced polymer (GFRP) face sheets, GFRP lattice webs, polyurethane (PU) foam and ceramsite filler. The vortexinduced vibration of three circular cylinders (each of diameter D) in an equilateral triangular arrangement is investigated using immersed boundary the method. Abdulrazzaq et al. (2020) investigated the thermoelastic buckling of small scale functionally graded material (FGM) nano-size plates with clamped edge conditions rested on an elastic substrate exposed to uniformly, linearly and non-linearly temperature distributions employing a secant function based refined theory. Material properties of the FGM nano-size plate have exponential gradation across the plate thickness. Civalek (2017) investigated the free vibration analysis of conical and cylindrical shells and annular plates made of composite laminated and functionally graded materials (FGMs). Carbon nanotubes reinforced (CNTR) composite case is also taken consideration for FGM. The equations of motion for conical shell are obtained via Hamilton's principle using the transverse shear deformation theory. Sharma et al. (2018a, b) studied the vibroacoustic responses of laminated composite curved panels subjected to harmonic point excitation in a combined temperature and moisture environment using a novel higher-order finite-boundary element model. The hygrothermal dependent composite material properties are incorporated macroscopically in the formulation. The natural frequencies alongside corresponding modes of the flat panels resting on an infinite rigid baffle are obtained by using finite element method in the framework of the higher-order shear deformation theory. Some valuable results regarding heat transfer of dusty fluid over a hollow stretching cylinder using multi-step DTM were reported (Rasekh et al. 2013). Conduction of dusty fluid flow along stretching cylinder with thermal conductivity and viscosity effects were dealt numerically (Konch and Hazarika 2017). Derakhshandeh1a et al. (2020) investigated the Reynolds number Re (= 50-200) effects on the flows around a single cylinder and the two tandem (center-to-center spacing  $L^* = L/D = 4$ ) cylinders, each of a diameter D. Vorticity structures, Strouhal numbers, and time-mean and fluctuating forces are presented and discussed. Sharma et al. (2017 a, b, c) investigated the vibro-acoustic responses of the laminated composite flat panel in an infinite rigid baffle under the influence of central and eccentric harmonic point excitation. A general mathematical model of the flat panel is developed in the framework of the higher order shear deformation theory to compute the vibrational properties. The frequency values of the panel are obtained by using simulation model through the commercial finite element package (ANSYS) via batch input technique. he structural responses are obtained using a



Fig. 1 The geometry of the cylinder

simulation model via ANSYS including the effect various geometries (cylindrical, elliptical, spherical and hyperboloid). Initially, the model has been established by solving adequate number of available examples to show the convergence and comparison behaviour of the natural frequencies. Salah et al. (2019) employed a simple fourvariable integral plate theory for examining the thermal buckling properties of functionally graded material (FGM) sandwich plates. The proposed kinematics considers integral terms which include the effect of transverse shear deformations. In some fresh attempts, the researchers have pondered over new dimensions of stretching i.e., exponentially stretching cylinder. The detailed study of flow and transfer of heat for hyperbolic tangent fluid over a stretching cylinder exponentially in vertical direction was carried out (Naseer et al. 2014). Shadravan et al. (2019) performed lateral load testing on seventeen wood wall frames in two sections. Section one included eight tests studying structural foam sheathing of shear walls subjected to monotonic loads following the ASTM E564 test method.

Similarity solution has been derived for steady boundary layer and heat flow of Casson nanofluid (Malik *et al.* 2013) while cylinder was stretching exponentially along its radius. The flow of Micropolar fluid through vertical exponentially stretching cylinder along the axial direction and discussed heat transfer effects, too, were considered (Rehman *et al.* 2015). Williamson fluid flow along an exponentially stretching cylinder was examined and they found its numerical solution (Iqbal *et al.* 2018). Recently some researcher used different methods for nonlinear modeling (Avcar 2019, Karami *et al.* 2017, 2018, Madani *et al.* 2016, Simsek 2011).

Open see softare (Moghaddam and Masoodi 2019), first order shear deformation theory (Loghman *et al.* 2018), MLPG method (Rad *et al.* 2020), Ritz-type variational method (Sofiyev *et al.* 2006), Multiphysical numerical (FE– BE) solution and higher-order shear theory (Sharma *et al.* 2019a, b, 2020 a, b).

The foremost intension of present study is to investigate the importance of dusty fluid flow in the field of fluid dynamics and the research in new dimension of stretching cylinder using Runge-Kutta method, which is our particular motivation. Many material researchers used different methodologies to investigate the structure of computational mechanics as: open see softare (Moghaddam and Masoodi, 2019), first order shear deformation theory (Loghman et al. 2018), MLPG method (Rad et al. 2020), Ritz-type variational method (Sofiyev et al. 2006), multiphysical numerical (FE-BE) solution and higher-order shear theory (Sharma et al. 2019a, b, 2020 a, b). The suggested method to investigate the flow and heat transfer effects of a dusty fluid along exponentially stretching cylinder is Runge-Kutta method, which is a well-known and efficient technique to develop the fundamental frequency equations. This method converge fastly than other methods. It is keenly seen from the literature, no evidence is found concerning current model. The transformed equations are solved numerically using Shooting technique with Runge-Kutta method. The influence of the physical parameters on the velocity and temperature profiles as well as the skin fraction coefficient and the local Nusselt number are examined in detail. The essential observations are as the fluid velocity decreases but temperature grows with rise in particle interaction parameter, and both the fluid velocity and temperature fall with increase in mass concentration parameter, Reynold number, Particle interaction parameter for temperature and the Prandtl number.

#### 2. Methodology

Consider laminar, steady, incompressible boundary layer flow of dusty viscous fluid in two dimensions along a hollow cylinder. The cylinder is stretching exponentially along positive z-axis with velocity  $U_w = 2ace^{z/a}$ , where c is the stretching rate. The origin of stationary cylindrical coordinate system has been positioned in the middle of the cylinder's leading edge, the z-axis is taken along the axis of the cylinder and the r-axis is assumed in the direction of radius of cylinder as shown in Fig. 1.

The flow of dust fluid is controlled by stretching of the cylinder and the surface temperature  $T_w = T_\infty + Ae^{(z/a)}$ . Both the dust particles and the fluid are taken initially to be in fixed position. We assume that particles of dust are in spherical form, having uniform size and constant number density. Under these suppositions along the Boussinesq and the boundary layer approximation the governing equations for the flow behavior are

$$\frac{\partial(rw)}{\partial z} + \frac{\partial(ru)}{\partial r} = 0, \tag{1}$$

$$w\frac{\partial w}{\partial z} + u\frac{\partial w}{\partial r} = v\left(\frac{\partial^2 w}{\partial r^2} + \frac{1}{r}\frac{\partial w}{\partial r}\right) + \frac{\gamma}{\tau_v}\left(w_p - w\right)$$
(2)

$$w_{p}\frac{\partial w_{p}}{\partial z} + u_{p}\frac{\partial w_{p}}{\partial r} = \frac{1}{\tau_{v}}\left(w - w_{p}\right)$$
(3)

$$\frac{\partial(rw_p)}{\partial z} + \frac{\partial(ru_p)}{\partial r} = 0, \qquad (4)$$

$$w\frac{\partial T}{\partial z} + u\frac{\partial T}{\partial r} = \alpha \left(\frac{\partial^2 T}{\partial r^2} + \frac{1}{r}\frac{\partial T}{\partial r}\right) +$$
(5)

$$\frac{\gamma}{\tau_{T}}(T_{p}-T)+\frac{\gamma}{c_{p}\tau_{v}}(w_{p}-w)^{2}$$

$$w_{p}\frac{\partial T_{p}}{\partial z} + u_{p}\frac{\partial T_{p}}{\partial r} = \frac{c_{p}}{c_{m}\tau_{T}}\left(T - T_{p}\right)$$
(6)

The components of velocity and temperature of fluid and the dust particles are (u, w, T) and  $(u_p, w_p, T_p)$ respectively in (r, z) directions. Parameter  $\gamma(=\frac{mN}{\rho})$ denotes the mass concentration of dust particles,  $\tau_v = \frac{m}{K}$ , is the relaxation time of particle phase and  $\tau_T$ , represents

the thermal equilibrium time, here  $\rho$ , v and  $\alpha$  are density, kinematic viscosity and thermal diffusivity of the fluid, respectively. Dusty fluid parameters K, N and m are the Stoke s resistance, number density and mass concentration of dust particle. Specific heat parameters of fluid and dust particles are denoted by  $c_p$  and  $c_m$ ,

respectively. The boundary conditions related to above system are

$$r = a; \quad w = U_w, \quad u = 0, \quad T = T_w = T_\infty + Ae^{(z/a)}$$
  

$$r \to \infty; \quad w = 0, \quad w_p = 0, \quad u_p = u, \quad (7)$$
  

$$T \to T_\infty, \quad T_p \to T_\infty.$$

Eqs. (1) and (6) are non-linear coupled PDEs. These equations can easily be transformed into set of ODEs by using similarity transformations.

$$\begin{aligned} \zeta &= \left(\frac{r}{a}\right)^2, \ u = -\frac{1}{2}U_w \frac{g(\zeta)}{\sqrt{\zeta}}, \\ w &= U_w g'(\zeta), \ \theta(\zeta) = \frac{T - T_\infty}{T_w - T_\infty}, \\ u_p &= -\frac{1}{2}U_w \frac{h(\zeta)}{\sqrt{\zeta}}, \\ w_p &= U_w h'(\zeta), \ \theta_p(\zeta) = \frac{T_p - T_\infty}{T_w - T_\infty}, \end{aligned} \tag{8}$$

The differentiation w.r.t  $\zeta$  is represented by prime. By employing the above similarity transformation Eqs. (1) and (4) are identically satisfied and other equations are transformed to

$$\zeta g''' + g'' + \operatorname{Re}\left(gg'' - g'^{2}\right) + \beta_{\nu} \gamma \left(h' - g'\right) = 0, \quad (9)$$

$$\operatorname{Re}(hh'' - {h'}^{2}) + \beta_{\nu}(g' - h') = 0, \qquad (10)$$

$$\zeta \theta'' + \theta' + \Pr \operatorname{Re}(g\theta' - g'\theta) + \Pr \gamma \beta_T (\theta_p - \theta)$$
  
+ 
$$\Pr \gamma \beta_{\nu} Ec (h' - g')^2 = 0,$$
 (11)

$$\operatorname{Re}\left(h'\theta_{p}-h\theta_{p}'\right)+\delta\beta_{T}\left(\theta_{p}-\theta\right)=0,$$
(12)

Where the non-dimensional parameters Re,  $\beta_{\nu}$ ,  $\gamma$ ,  $\beta_{T}$ , Pr, Ec,  $\beta_{T}$ ,  $\delta$  and  $\delta$  are defined as

$$\beta_{\nu} = \frac{a^2}{4\nu\tau_{\nu}}, \gamma = \frac{mN}{\rho}, \operatorname{Re} = \frac{aU_w}{4\nu},$$

$$Ec = \frac{U_w^2}{c_p(T_w - T_{\infty})}, \operatorname{Pr} = \frac{\nu}{\alpha}, \beta_T = \frac{a^2}{4\nu\tau_T}, \delta = \frac{c_p}{c_m},$$
(13)

Here,  $\beta_{\nu}$  is fluid particle interaction parameter,  $\gamma$  is mass concentration parameter, Re is the Reynold number, *Ec* is the Eckert number, Pr is the Prandtl number,  $\beta_T$ *is* the fluid-particle interaction parameter for temperature and  $\delta$  *is* the specific ratio, respectively. The transformed boundary conditions are



Fig. 2 Impact of particle interaction parameter on profile of velocity



Fig. 3 Impact of mass concentration parameter on profile of velocity

$$g(1) = 0, g'(1) = 1, g'(\infty) = 0, \theta(1) = 1.$$
  

$$h'(\zeta) = 0, h(\zeta) = g(\zeta), \theta(\zeta) = 0, \quad (14)$$
  

$$\theta_p(\zeta) = 0 \text{ as } \zeta \to \infty.$$

The skin friction coefficient  $C_f$  and the Nusselt number Nu are defined as

$$C_{f} = \frac{\tau_{w}}{\rho U_{w}^{2}/2},$$
 (15)

$$Nu = \frac{aq_w}{k(T_w - T_\infty)},$$
(16)

where  $\tau_w$  and  $q_w$  are the shear stress and rate of heat transfer, respectively. These quantities are defined by

$$\tau_w = \mu(\frac{\partial w}{\partial r})\Big|_{r=a},\tag{17}$$

$$q_{w} = -k\left(\frac{\partial T}{\partial r}\right)\Big|_{r=a},$$
(18)

Using the similarity transformation (8) in Eqs. (17) and (18) and substituting it in Eqs. (15) and (16), the dimensionless skin friction coefficient and Nusselt number are achieved like

$$C_f \operatorname{Re} = g^n(1) \tag{19}$$



Fig. 4 Impact of Reynold number on profile of velocity



Fig. 5 Impact of particle interaction parameter on profile of temperature

$$Nu/2 = -\theta'(1) \tag{20}$$

Eqs. (9) - (12) are non-linear coupled ODEs. Exact analytical solution of above equations are not possible, therefore in the coming section numerical results of the problem are discussed and presented.

#### 3. Results and discussion

Numerical solution of Eqs. (9) - (12) along with boundary condition (14) is attained through shooting method with RK-6. Consequences of the impact of particle interaction parameter  $\beta_{\nu}$ , the mass concentration parameter  $\gamma$  and the local Reynold number *Re* over the velocity profile of fluid and dust phase are elaborated with graphical Figs. 2-4 while Figs. 5-11 show the variation of particle interaction parameter  $\beta_{\nu}$ , the mass concentration parameter  $\gamma$ , local Reynold number *Re*, particle interaction parameter for temperature  $\beta_{T}$ , the Eckert number *Ec*, the prandtl number *Pr* and the specific ratio  $\delta$  over the temperature profile.

Fig. 2 represents the profile of the velocity for various non-identical values of the particle interaction parameter for phases of fluid and dust. It is seen in the graph that velocity of dust phases increases for large values of particle



Fig. 6 Impact of mass concentration parameter on profile of temperature



Fig. 7 Impact of Reynold number on profile of temperature

interaction parameter while there is fall in velocity for fluid phase. In fact, by increasing the fluid-particle interaction parameter the fluid and dust particles interaction also increases so the dust phase velocity enhances until the relative velocity of the fluid and particle phase become identical. On the other hand, increasing the fluid-particle interaction parameter the suspension of dust particles is increased that produces an internal friction within the fluid as a result the fluid phase velocity decreases. In Fig. 3, it is clearly shown that velocity decreases for both the fluid and dust phases on increasing the mass concentration parameter. The reason is that; more mass concentration will result in increase in viscosity which ultimately reduces the velocity. While in Fig. 4, impact of local Reynold number (*Re*) on profile of the velocity of both dust and fluid phases is shown graphically. It is obvious from the figure that by increasing the Reynold number (*Re*) viscous forces dominates, and velocity decreases in both the phases. In Figs. 2-4 the values of parameters are taken as  $\beta_v = 2$ ,  $\gamma = 1$ & *Re* =10. The variation of skin friction coefficient -g''(1)with local Reynold number *Re*, particle interaction parameters  $\beta_v$  and the mass concentration parameter  $\gamma$  has been tabulated in Table 1. It is evident that skin friction coefficient is found to increase for increasing values of *Re*,  $\beta v$  and  $\gamma$ . Because, rise in *Re* increases viscous forces which ultimately increases skin friction coefficient, similarly increasing dusty fluid parameters produces higher resistance



Fig. 8 Impact of particle interaction parameter of temperature on profile of temperature



Fig. 9 Impact of Prandtl number on profile of temperature

to the flow and then skin friction is also increased. Fig. 5, depicts the impact of particle interaction parameter on temperature profile. A noticeable increase is observed in temperature for higher values of  $\beta_{\nu}$ . Here collision rate goes up and in turns kinetic energy (K.E) increases. K.E has direct relation to the temperature. So, increase in particle interaction results in high temperature for both the fluid and the dust phases. Fig. 6 gives a graphical picture of variation in mass concentration parameter over temperature profile. Higher values of  $\gamma$ , results in more number of dust particles which in turns slow down the velocity. So, ultimate result is reduction in heat transfer rate for both the phases of fluid. Decrease in temperature profile is noted in Fig. 7 for

increasing values of *Re* for both the phases. As *Re* is in inverse relation with viscosity, there is a decrease in friction factor which produces depreciation in temperature. Growing values of particle interaction parameter give rise in the velocity of the dust and fluid particles until both acquire the same velocity, then more collision enhances the temperature of the dust phase. But at this moment, another prominent change occur i.e., increase in suspension of dust particles which slows down the fluid so finally temperature drops for the fluid phase as depicted in Fig. 8. Behavior of Prandtl number on profile of temperature is shown in Fig. 9. In physical sense, Prandtl number has inverse relation with thermal diffusivity, so weak diffusion of heat energy is



Fig. 10 Impact of Eckert number on profile of temperature



Fig. 11 Impact of specific ratio on profile of temperature

observed for ascending Pr, which consequently lowers down the temperature. Fig. 10 response of Eckert number on profile of temperature is exhibited. Temperature goes up for both the dust and the fluid phases by increasing the *Ec*. It can be justified by keeping in view that *Ec* enhances bouncy forces in the fluid which increase the collision of particles. Through collision more energy is accumulated in fluid and temperature is raised. Specific ratio is the required heat energy to raise unit temperature of unit substance. It means at high specific ratio more heat energy is provided, logically temperature goes high for both the dust and the fluid phases as shown in Fig. 11. In Table 2 (a) and (b), Nusselt number decreases for larger values of Re,  $\gamma$ ,  $\beta_T$  and Pr, while inverse behavior is observed for  $\beta_{\nu}$ , Ec and  $\delta$ . Such behavior is justified as Nesselt number goes high with increasing temperature. Ultimately convictive heat transfer occurs with rising temperature. Same trend has been followed in case  $\beta_{\nu}$ , Ec and  $\delta$  where notable increase in Nesselt number is seen. While inverse mood of Re,  $\gamma$ ,  $\beta_T$ and Pr is observed due to the same reason.

	· / · /	0 ( )		
Re	$\beta_{v}$	γ	-g"(1)	
5	2	1	2.741649	
10			3.612068	
15			4.287201	
30			5.834313	
50			7.392431	
10	0.1		3.364133	
	0.2		3.379972	
	0.5		3.425116	
	1		3.493254	
	2		3.612082	
		0.1	3.374806	
		0.2	3.401936	
		0.5	3.481566	
		0.7	3.533639	
		1.0	3.612082	

Table 1 For different values of *Re*,  $\beta_v$  and  $\gamma$  numerical value of g''(1)

Table 2a For various values of  $\operatorname{Re}, \beta_{\nu}, \gamma, \beta_{T}, \operatorname{Pr}, Ec$  and  $\delta$  numerical values of  $-\theta'(1)$ 

Re	$eta_v$	γ	$eta_{\scriptscriptstyle T}$	Pr	Ec	$\delta$	$-\theta'(1)$
5	2	1	2	1	0.5	0.5	2.718925
10							3.564225
15							4.234356
30							5.784181
50							7.348750
10	0.1						3.687892
	0.2						3.678863
	0.5						3.653923
	1						3.618422
	2						3.564225
		0.1					3.367754
		0.2					3.390304
		0.5					3.456823
		0.7					3.500279
		1.0					3.564225

# 4. Conclusions

The laminar boundary layer flow behavior and heat transfer of dusty viscous fluid in two dimensions subject to the steady, incompressible conditions has been studied numerically. The impact of different physical parameters on velocity and temperature profile is discussed and shown graphically.

Some significant points are as follows: -

1. An increase in velocity is noted for dust phase while there is a decrease in the phase of fluid for the impact of particle interaction parameter  $\beta_{v}$ .

2. A considerable rise in the velocity profile for both the dust and fluid phases is seen with the impact of mass concentration parameter  $\gamma$ .

3. For local Reynold number Re effect a notable decrease in velocity for dust and fluid phases is observed.

4. All the parameters i.e., particle interaction  $\beta_{\nu}$ , mass concentration  $\gamma$  & Reynold number (Re) enhance skin friction coefficient.

Re	$\beta_{v}$	γ	$\beta_{T}$	Pr	Ec	δ	$-\theta'(1)$
10	2	1	0.1	1	0.5	0.5	3.218158
			0.2				3.240484
			0.5				3.303769
			1				3.399314
			2				3.564225
				0.7			2.903240
				1			3.564225
				3			6.537192
				5			8.574081
				7			10.224347
					0		3.637020
					0.2		3.607902
					0.4		3.578784
					0.6		3.549666
					0.8		3.520548
						0.1	3.593417
						0.3	3.578280
						0.5	3.564225
						0.7	3.551147
						0.9	3.538953

Table 2b For various values of Re,  $\beta_{\nu}$ ,  $\gamma$ ,  $\beta_{T}$ , Pr, Ec and  $\delta$  numerical values of  $-\theta'(1)$ 

5. Temperature of the fluid increases for both the phases for ascending values of particle interaction parameter ( $\beta_{\nu}$ ).

6. Reduction of temperature is reported for the larger values of mass concentration parameter ( $\gamma$ ).

7. Increase in Reynold number (Re) results in fall of temperature.

8. Larger values of particle interaction parameter for temperature  $(\beta_T)$  boost up the temperature of dust phase while decreases for the fluid phase.

9. Decline in temperature is noted for high values of Prantl number (Pr).

10. Temperature increases with the increase of Eckert number (Ec).

11. Impact of increasing specific ratio ( $\delta$ ) is also in ascending order for temperature.

12. Local Nusselt number increases with parameter  $\beta_{v}$ , *Ec and*  $\delta$  whereas showing opposite relation in case of Re,  $\gamma$ ,  $\beta_{r}$  and Pr ...

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